



## **pH variation and influence in an autotrophic nitrogen removing biofilm system**

An efficient numerical solution strategy

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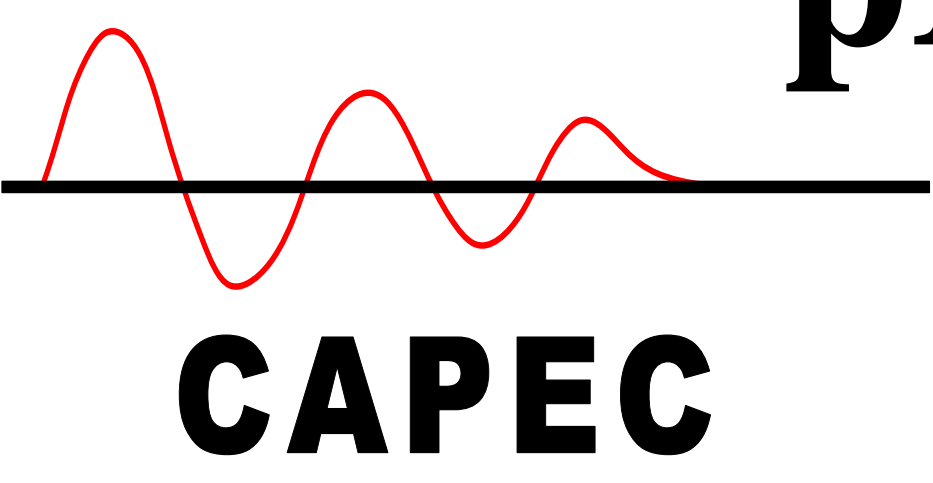
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# pH variation and influence in an autotrophic nitrogen removing biofilm system:

## An efficient numerical solution strategy



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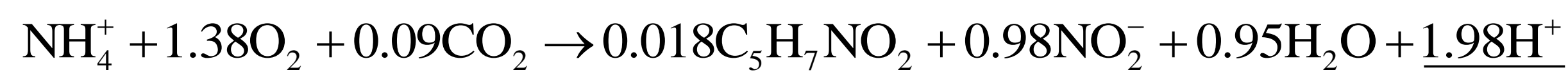
### 1. Introduction

pH impacts the nitrification and anammox processes and vice versa through:

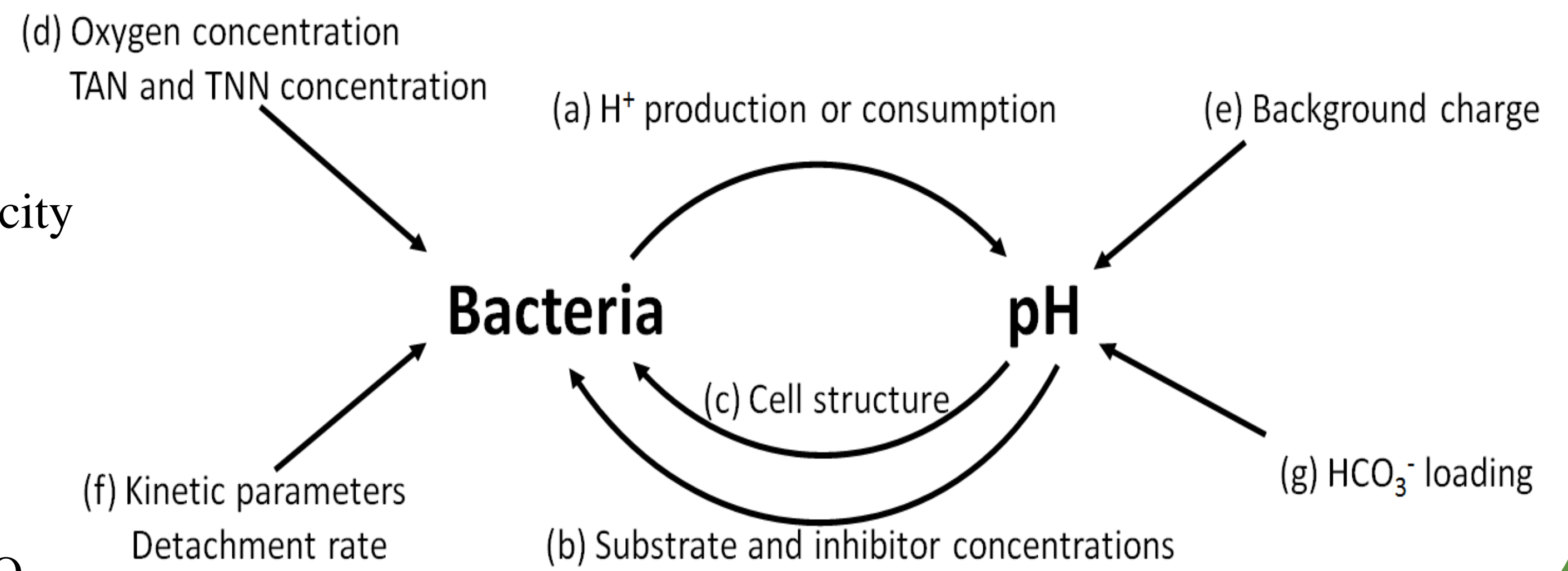
(a) H<sup>+</sup> production/consumption, (b) substrate and inhibitor speciation, (c) cell structure dependency, (d) substrate and inhibitor concentrations, (e) system background charge and distribution, (f) microbial activity, and (g) buffering capacity

#### Stoichiometry of microbial processes

##### Nitrification:

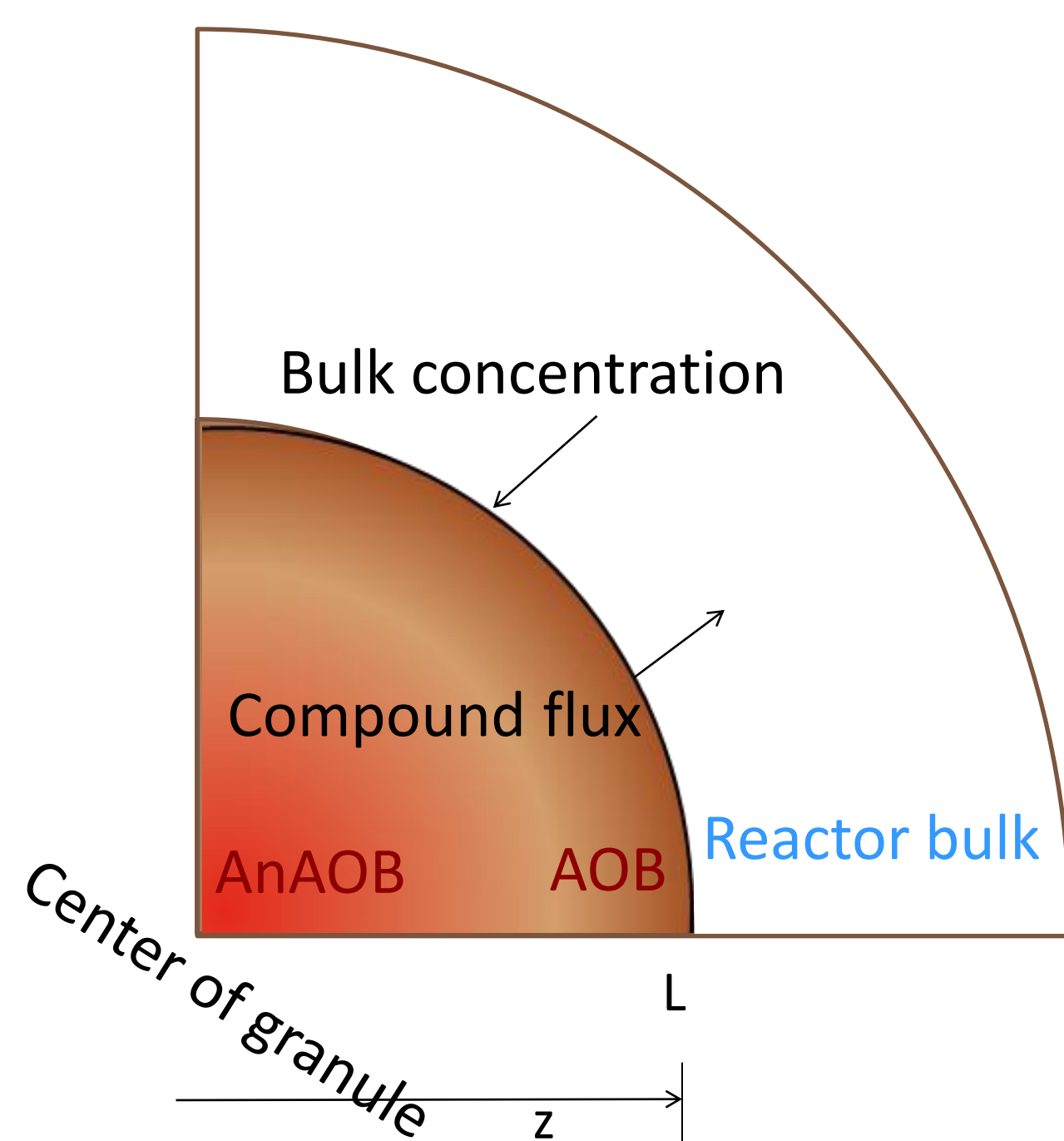


##### Anammox:



### 2. Methods and solution strategy

#### Model description



#### Biofilm mass balance

$$\frac{\partial(C_i V)}{\partial t} = \frac{\partial(j_i A)}{\partial z} dz + r_i dV$$

#### Reactor mass balance

$$\frac{dC_{i,bulk}}{dt} = \frac{Q_{in}C_{i,in} - Q_{out}C_{i,bulk}}{V_{react}} - j_{Ci} \frac{A}{V_{react}} + r_{i,bulk}$$

i = soluble or particulate compound

j = substrate flux

z = radial distance from the center of the granule

r<sub>i</sub> = microbial growth and conversion

Q = flow

V<sub>react</sub> = reactor volume

A = biofilm surface area

#### New and fast numerical solution for pH calculation

A system of nine nonlinear equations was solved by a multi-dimensional Newton-Raphson method adapted from Luff et al. (2001) coupled with the granular biofilm model (left).

$$0 = \text{TAN} - (\text{NH}_4^+ + \text{NH}_3)$$

$$0 = \text{TNN} - (\text{HNO}_2 + \text{NO}_2^-)$$

$$0 = \text{TIC} - (\text{CO}_2 + \text{HCO}_3^- + \text{CO}_3^{2-})$$

$$0 = K_w - \text{OH}^- \cdot \text{H}^+$$

$$0 = K_{e,\text{NH}_4} \cdot \text{NH}_4^+ - \text{NH}_3 \cdot \text{H}^+$$

$$0 = K_{e,\text{HNO}_2} \cdot \text{HNO}_2 - \text{NO}_2^- \cdot \text{H}^+$$

$$0 = K_{e,\text{CO}_2} \cdot \text{CO}_2 - \text{HCO}_3^- \cdot \text{H}^+$$

$$0 = K_{e,\text{HCO}_3} \cdot \text{HCO}_3^- - \text{CO}_3^{2-} \cdot \text{H}^+$$

$$0 = Z^+ - \text{NO}_3^- - \text{HCO}_3^- - 2 \cdot \text{CO}_3^{2-} - \text{NO}_2^- - \text{OH}^- + \text{NH}_4^+ + \text{H}^+$$

Because the above system was computationally heavy to solve and prone to errors, the pH was determined offline for the complete expected range of TAN, TNN, TIC and NO<sub>3</sub><sup>-</sup>, prior to simulation. A lookup table was therefore constructed using multi-dimensional interpolation tools in the Matlab software.

Four scenarios representing different operating points were defined and simulated:

(1) Default (2) High oxygen loading (3) Smaller granules (4) High strength wastewater → N and oxygen loadings

### Findings

- pH solver was successfully constructed and implemented in the MATLAB software.

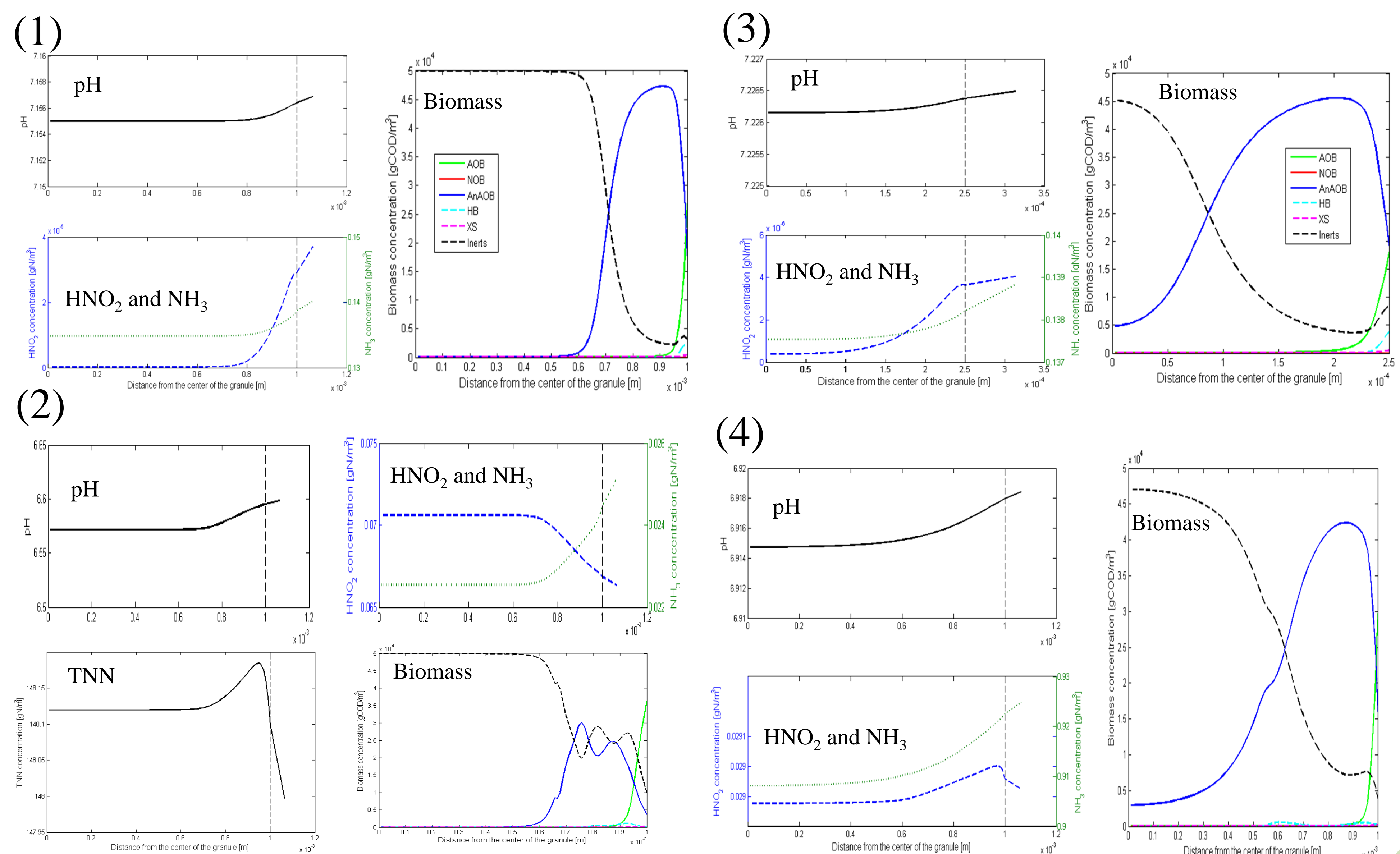
- Approximations of cell structure dependency on pH and the value of the background charge were needed to solve the model.

- The predicted pH profile showed decreasing pH with increasing depth into the biofilm in all scenarios, due to AOB presence in the outer layers.

- The background charge was found to have a great impact on the value and shape of the pH profile.

- More info on background charge effect and cell structure dependency, supported by experiments, is needed to make further progress.

### 3. Results and discussion



#### References:

1. R. Luff et al. Comput. Geosci. **27**(2), 157-169 (2001).

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